

### Answer Key's

|    |   |    |   |    |   |    |   |    |   |    |   |    |   |
|----|---|----|---|----|---|----|---|----|---|----|---|----|---|
| 1  | A | 2  | D | 3  | B | 4  | A | 5  | C | 6  | C | 7  | D |
| 8  | B | 9  | C | 10 | C | 11 | D | 12 | B | 13 | D | 14 | C |
| 15 | D | 16 | B | 17 | A | 18 | C | 19 | A | 20 | A | 21 | D |
| 22 | D | 23 | B | 24 | B | 25 | C | 26 | A | 27 | B | 28 | A |
| 29 | D | 30 | B | 31 | B | 32 | C | 33 | C | 34 | C | 35 | D |
| 36 | B | 37 | C | 38 | B | 39 | B | 40 | B | 41 | B | 42 | C |
| 43 | D | 44 | D | 45 | C | 46 | C | 47 | D | 48 | C | 49 | C |
| 50 | B | 51 | A | 52 | C | 53 | C | 54 | C | 55 | A | 56 | A |
| 57 | B | 58 | A | 59 | D | 60 | C | 61 | A | 62 | C | 63 | C |
| 64 | B | 65 | A | 66 | C | 67 | B | 68 | B | 69 | D | 70 | D |
| 71 | A | 72 | C | 73 | B | 74 | A | 75 | D | 76 | A | 77 | A |
| 78 | A | 79 | C | 80 | B | 81 | D | 82 | A | 83 | B | 84 | C |
| 85 | A |    |   |    |   |    |   |    |   |    |   |    |   |

### Explanation:-

7. Option (a) is not correct because if heat flows from the system, entropy of the system will decrease, and the entropy of environment will increase. Sum of the entropy of system and environment i.e. the entropy of universe can not be negative but entropy of system can be negative

8.  $dy = \left(1 - \frac{1}{x^2 + 1}\right) dx$ , Integrating,  $y = x - \tan^{-1} x + C$ ,  $y(0) = 0 \therefore C = 0, \therefore f(1) = 1 - \tan^{-1} 1 = 1 - \frac{\pi}{4}$

9. A and B are independent events

$$P(A \text{ or } B) = P(A) + P(B) - P(A \cap B) = P(A) + P(B) - P(A)P(B) = \frac{6}{36} + \frac{6}{36} - \frac{6}{36} \times \frac{6}{36} = \frac{11}{36}$$

10.  $\begin{vmatrix} \lambda & 3 & -5 \\ 2 & -4\lambda & \lambda \\ -4 & 18 & 7 \end{vmatrix} = 0, \lambda = -3 \text{ or } 1$

11.  $\lim_{x \rightarrow 1^+} \frac{x^2 - 1}{|x - 1|} = 2, \lim_{x \rightarrow 1^-} \frac{x^2 - 1}{|x - 1|} = -2$  doesn't exist

13.  $\lambda = \frac{9}{5} = 1.8, \mu = \frac{10}{5} = 2, L_q = \frac{\lambda^2}{\mu(\mu - \lambda)} = 8.1$

14.  $q_0 = \sqrt{\frac{2C_3 R}{C_1}} = 1000 \text{ units}, \text{ Length of cycle} = t_0 = \frac{1000}{100} = 10 \text{ days}$

As lead time is 13 days and cycle length is 10 days

Reorder point =  $(13 - 10) \times 100 = 300 \text{ units}$

17. Option b is not correct because, it does not include open cycle gas turbines which also consider as IC engines where combustion takes place in separate combustion chamber. So the most appropriate answer is (a)

19. Unit power,  $P_u = \frac{P}{H^{3/2}}$ , Unit discharge,  $Q_u = \frac{Q}{\sqrt{H}}$

$$\text{Ratio} = \frac{P_u}{Q_u} = \frac{P \times \sqrt{H}}{H^{3/2} \times Q} = \frac{P}{QH} = 4000$$

20. Mach Velocity,  $C = \sqrt{\frac{K}{\rho}} = \sqrt{\frac{15600 \times 9.81 \times 10^4}{0.8 \times 1000}} = 1383 \text{ m/s}$

21. 
$$\begin{vmatrix} -1 & \cos C & \cos B \\ \cos C & -1 & \cos A \\ \cos B & \cos A & -1 \end{vmatrix} \xrightarrow[\substack{R_{21}(\cos C) \\ R_{31}(\cos B)}]{} \begin{vmatrix} -1 & \cos C & \cos B \\ 0 & 0 & \cos A + \cos C \cos B \\ 0 & \cos B \cos C + \cos A & \cos^2 B - 1 \end{vmatrix}$$

$$= -\left[\sin^2 B \sin^2 C - \{(-\cos(B+C) + \cos B \cos C)\}^2\right], [\because A+B+C = \pi] = -[\sin^2 B \sin^2 C - \sin^2 B \sin^2 C] = 0$$

22. The corresponding augmented matrix

$$\begin{pmatrix} 1 & -2 & 3 & 3 \\ 2 & 1 & -1 & 9 \\ -3 & -4 & 5 & -8 \end{pmatrix} \xrightarrow[\substack{-2R_1+R_2 \\ 3R_1+R_3}]{} \begin{pmatrix} 1 & -2 & 3 & 3 \\ 0 & 5 & -7 & 3 \\ 0 & -10 & 14 & 1 \end{pmatrix}$$

$$\downarrow 2r_2 + r_3$$

$$\begin{pmatrix} 1 & -2 & 3 & 3 \\ 0 & 5 & -7 & 3 \\ 0 & 0 & 0 & 7 \end{pmatrix}$$

The bottom row of the final matrix corresponds to the equation,  $0.x + 0.y + 0.z = 7$ , which has no solution

23.  $\frac{dy}{dx} = \frac{2x}{y^2 + 1} \Rightarrow (y^2 + 1)dy - 2xdx = 0$ , The above equation is exact.

Integrating we get,  $\frac{y^3}{3} + y - x^2 = C$ , At  $(1, 2)$ ,  $C = \frac{11}{3}$ .  $\therefore$  The integral curve is  $y^3 + 3y - 3x^2 = 11$

24.  $P\left(X \leq \frac{1}{3}\right) = F_x\left(\frac{1}{3}\right) = 1 + e^{\frac{2}{3}} = 2.95$

25.  $\lim_{x \rightarrow \infty} (3^x + 3^{2x})^{1/x} = \lim_{x \rightarrow \infty} \left[ 9^x \cdot \left( \frac{3^x}{9^x} + 1 \right) \right]^{1/x} = \lim_{x \rightarrow \infty} \left[ 9 \cdot \left\{ \left( \frac{1}{3} \right)^x + 1 \right\}^{1/x} \right] = 9$

26.  $f(x) = 3x - \cos x - 1, f'(x) = 3 + \sin x, x_{n+1} = x_n - \frac{f(x_n)}{f'(x_n)} = \frac{x_n \sin x_n + \cos x_n + 1}{3 + \sin x_n}$

Let  $x_0 = 0.6$ , First approximation:  $x_1 = \frac{x_0 \sin x_0 + \cos x_0 + 1}{3 + \sin x_0} = \frac{0.6 \sin(0.6) + \cos(0.6) + 1}{3 + \sin(0.6)} = 0.6071$

Second approximation:

$$x_2 = \frac{0.6071 \sin 0.6071 + \cos 0.6071 + 1}{3 + \sin(0.6071)} = 0.6071$$

$$27. \quad L\left(\frac{f(t)}{t}\right) = \int_s^\infty \bar{f}(s) ds \quad \text{where } \bar{f}(s) = L(f(t)), \quad L\left(\frac{\sin t}{t}\right) = \int_s^\infty \frac{1}{1+s^2} ds = \cot^{-1} s, \quad L\left(e^t \left(\frac{\sin t}{t}\right)\right) = \cot^{-1}(s-1)$$

28-29. From Merchant's circle

$$F_s = F_c \cos \phi - F_t \sin \phi = 248.3 \text{ N}, \quad F_s = \frac{w t_1 \tau_s}{\sin \phi} \Rightarrow t_1 = 0.14 \text{ mm}, \quad \frac{\sin \phi}{\cos(\phi - \alpha)} = \frac{t_1}{t_2}, \therefore \alpha = 16.67^\circ$$

$$31-32. \sum F_x = 0, \sum F_y = 0$$

$$T_{AC} \cos 30^\circ + F \cos \alpha = T_{BC} \cos 45^\circ, \quad F \sin \alpha + T_{AC} \sin 30^\circ + T_{BC} \sin 45^\circ = 0$$

$$33. \quad \eta = \frac{P}{\rho g \times Q \times H} \Rightarrow H = 7 \text{ m}, \text{ Specific speed } N_s = \frac{N \sqrt{P}}{H^{\frac{5}{4}}}$$

$$35. \quad \text{Heat transfer from oil} = C_h \Delta T = 2000(425 - 350) = 150 \text{ KW}$$

for parallel flow arrangement

$$\Delta T_1 = T_{hi} - T_{ci} = 400^\circ \text{C}, \quad \Delta T_2 = T_{ho} - T_{co} = 150^\circ \text{C}$$

$$\Delta T_{lm} = \frac{\Delta T_1 - \Delta T_2}{\ln(\Delta T_1 / \Delta T_2)} = 254.88^\circ \text{C}, \quad \text{Heat exchanger area } A_1 = \frac{Q}{U \Delta T_{lm}} = .735 \text{ m}^2$$

$$\text{For counter flow arrangements, } \Delta T_1 = T_{hi} - T_{co} = 225^\circ \text{C}, \quad \Delta T_2 = T_{ho} - T_{ci} = 325^\circ \text{C}$$

$$\Delta T_{lm} = \frac{\Delta T_1 - \Delta T_2}{\ln \Delta T_1 / \Delta T_2} = 271.94^\circ \text{C}, \quad A_2 = \frac{Q}{u \Delta T_{lm}} = .689 \text{ m}^2, \quad A_1 / A_2 = 1.067$$

(Area required in parallel flow heat exchanger is always more than counter flow heat exchanger. Here only 1 option has the ratio more than 1. So it can be attempted without solving the whole problem)

$$37. \quad \text{Co-efficient of steadiness} = \frac{N_1 + N_2}{2(N_1 - N_2)}, \quad \text{where } N_1 = \text{maximum speed}$$

$$N_2 = \text{minimum speed, Maximum fluctuation of speed} = N_1 - N_2 = 30.61 \text{ rpm}$$

$$38-39. f_p = \text{Permissible stress for pinion} = 140$$

$$y_p = \text{tooth factor for pinion} = .154 - \frac{.912}{50} = .13576$$

$$\text{Strength factor for Pinion} = f_p \times y_p = 140 \times .13576 = 19$$

$$\text{Similarly } f_g = 115 \text{ N/mm}^2$$

$$y_g = .154 - \frac{.912}{75} = .14184$$

$$\text{Strength factor for gear} = f_g \times y_g = 115 \times .14184 = 16.31$$

So, Lewis equation will be used for gear since strength factor is low.

$$40. \quad \epsilon = 1 - \frac{2h_0}{c} = D - d$$

$$41. \quad \theta = 270^\circ = 4.712 \text{ rad}, \quad \frac{T_1}{T_2} = e^{\mu\theta} = 3.25, \quad T_1 = 3.25 T_2, \quad T_B = (T_1 - T_2)r_e$$

$$re = r + \frac{t}{2} = 300 + .005 \times \frac{600}{2} = 300.15 \text{ Nmm}, \quad 1575 = (3.25T_2 - T_2) \times 300.15 \times 10^{-3}$$

$$42. \quad \frac{\ell}{K} = 75 \text{ for both ends hinged}, \quad \frac{L}{K} = \frac{\ell}{\sqrt{2}K} \text{ for one end fixed and one hinged length} = \frac{\ell}{\sqrt{2}}$$

$$\% \text{ change} = \frac{75 - \frac{75}{\sqrt{2}}}{75} \times 100 = 29.28\%$$

$$43. \quad e_1 = \text{circumferential strain} = \frac{\delta d}{d} = \frac{3}{100} = .03, \quad e_2 = \text{longitudinal strain} = \frac{\delta \ell}{\ell} = \frac{5}{100} = .05$$

$$\text{change in volume } \delta v = v(e_2 + 2e_1) = 8.25 \text{ cm}^3$$

46. For 1-2-3-5-7-9-10 to be critical path, summation of time for all the activities along the path should be maximum.

$$47. \quad \sigma^2 = \left( \frac{t_p - t_o}{6} \right)^2 = \left( \frac{10 - 4}{6} \right)^2 = 1$$

$$50. \quad \frac{\partial T}{\partial x} = -75 + 16x + 36x^2 - 28x^3$$

Heat energy stored in unit time = Heat entering - Heat leaving

$$\text{Heat entering, } Q_0 = -kA \left( \frac{\partial T}{\partial x} \right)_{x=0} = 450 \text{ W},$$

$$\text{Heat leaving, } Q_2 = -kA \left( \frac{\partial T}{\partial x} \right)_{x=1.2} = 314.054 \text{ W}$$

$$\text{Heat energy stored} = 73.728 \text{ W}, \quad \frac{\partial^2 T}{\partial x^2} = 16 + 72x - 84x^2$$

$$\text{rate of temperature change at entry side } k, \quad \frac{\partial T}{\partial t} = \alpha \left( \frac{\partial^2 T}{\partial x^2} \right)_{x=0} = 28.32 \times 10^{-3} \text{ }^\circ\text{C/h}$$

$$\text{rate of temperature change at exit side}, \quad \frac{\partial T}{\partial t} = \alpha \left( \frac{\partial^2 T}{\partial x^2} \right)_{x=1.2} = -32.85 \times 10^{-3} \text{ }^\circ\text{C/h}$$

for rate of heating or cooling to be maximum

$$\frac{\partial}{\partial x} \left( \frac{\partial T}{\partial t} \right) = 0, \quad \alpha \frac{\partial}{\partial x} \left( \frac{\partial^2 T}{\partial x^2} \right) = 0, \quad \text{i.e. } \frac{\partial^3 T}{\partial x^3} = 0, \Rightarrow 72 - 168x = 0, \quad x = 0.428 \text{ m}$$

$$51. \quad \frac{P_2}{P_1} = \left( \frac{V_1}{V_2} \right)^2, \quad P_2 = \left( \frac{6000}{2000} \right)^2 \times 100 = 900 \text{ kPa}, \quad dw = \int_{V_1}^{V_2} P dv, \quad Pv^2 = c, \quad P = \frac{c}{V^2}, \quad dw = \int_{V_1}^{V_2} \frac{c}{V^2} dv = c \left[ -\frac{1}{V} \right]_{V_1}^{V_2}$$

$$w = P_1 V_1 - P_2 V_2 = (100 \times 6000 \times 10^3 \times 10^{-6} - 900 \times 10^3 \times 2000 \times 10^{-6}) = -1200 \text{ J} = -1.2 \text{ kJ}$$

$$53. \quad (\Delta U)_{ACB} = (\Delta U)_{ADB}, \quad \Delta Q = \Delta U + \Delta w$$

$$55. \quad 0.4 = W / Q_1, \quad W = 0.4Q_1, \quad \text{COP} = Q_3 / W, \quad \text{COP} = 2Q_1 / 0.4Q_1 = 5$$

$$56. \quad \delta - \Delta = \frac{P\ell}{A\epsilon}, \delta\ell\Delta T = \Delta + \frac{P\ell}{A\epsilon} \quad P = \sigma A, \ell\alpha\Delta T = \Delta + \frac{\sigma\ell}{\epsilon}, \Delta T = \frac{\Delta}{\ell\alpha} + \frac{\sigma}{\epsilon\alpha}, \quad \Delta T = 70.6^\circ\text{C}, T = \Delta T + T_0 = 50.6^\circ\text{C}$$

$$57. \quad \text{for 1st bar, stress} = \frac{P}{\frac{\pi}{4}(2d)^2} = \frac{P}{\pi d^2}, \text{strain energy stored} = \frac{F^2}{2E} \times \text{vol of bar} = \frac{P^2\ell}{2E\pi d^2}$$

$$2^{\text{nd}} \text{ bar, } AB = F_1 = \frac{4P}{\pi d^2}, BC = F_2 = \frac{P}{\pi d^2}$$

$$\text{stress energy} = AB+BC = \frac{f_1^2}{2E} \times \text{vol. of AB} + \frac{f_2^2}{2E} \times \text{vol. of BC} = \frac{\pi^2\ell}{E\pi d^2}, \text{ratio} \rightarrow 1/2$$

$$59. \quad \omega_h = \sqrt{\frac{s}{m}} = 24.49 \text{ rad/sec}, \frac{x_0}{x_2} = \frac{x_0}{x_1} \times \frac{x_1}{x_2} = \left(\frac{x_0}{x_1}\right)^2, \frac{x_0}{x_1} = \left(\frac{x_0}{x_2}\right)^{1/2} = \left(\frac{45}{8}\right)^{1/2} = 2.37$$

$$\frac{2\pi\xi}{\sqrt{1-\xi^2}} = \ell n 2.37 = 0.867, \Rightarrow \xi = 0.136, C = 2m\omega_h\xi = 0.4 \text{ N/mm/sec.}$$

$$60. \quad \text{Cycle } \eta = \frac{Q - 0.56Q}{Q} = 44\%$$

$$\text{Gen.output} = 0.92 \times 0.94 \times 0.44 \times 0.95Q \text{ \& net output} = (1 - 0.06) \text{ gen.output}$$

$$\text{overall } \eta = 0.92 \times 0.94 \times 0.95 \times 0.94 \times 0.44 = 0.34 \Rightarrow 34\%$$

$$63. \quad A_s = A_c, 4\pi r^2 = 6a^2 \Rightarrow r^2 = \frac{6}{4\pi} a^2, (t_s)_{\text{sphere}} = k \left( \frac{V_s}{A_s} \right)^2, (t_s)_{\text{cube}} = k \left( \frac{V_c}{A_c} \right)^2, \frac{(t_s)_s}{(t_s)_c} = \left( \frac{4}{3}\pi \right)^2 \frac{(r^2)^3}{(a^2)^3} = 1.9$$

$$65. \quad L = \sqrt{R(h_o - h_f)} = 1.55 \text{ in, true strain } \epsilon = \ln \left( \frac{1.00}{0.80} \right) = 0.223, \text{roll force } F = Lw\gamma_{\text{average}} = 1.6 \text{ MN}$$

$$\text{Power} = \frac{2\pi FLN}{33,000} = 670 \text{ kW} \times \text{two rolls} = 1340 \text{ kW}$$

$$66. \quad dQ = dU + dW \text{ is only valid for closed system and gas turbine and steam turbines are open systems.}$$

$$67. \quad \text{Average BP for 3 cylinder} = \frac{2\pi NT}{60000} = 13.82 \text{ kW, average IP with 1 cylinder} = 20 - 13.82 = 6.18 \text{ kW}$$

$$\text{total IP} = 4 \times 6.18 = 24.72 \text{ kW, ISFC} = \text{bsfc} \times \frac{\text{BP}}{\text{IP}} = 291.26 \text{ g/kWh, fuel consumption} = \frac{\text{ISFC} \times \text{IP}}{360 \times 1000} = 2 \times 10^{-3} \text{ kg/S}$$

$$69. \quad \text{It must be remembered that velocity and pressure head behave in reverse fashion. Thus velocity will be maximum for least area and pressure will be minimum. } \therefore D \rightarrow 3, 1, 2, 4.$$

$$70. \quad \text{Torque} = \text{Shear stress} \times \text{Surface area} \times \text{Torque arm}$$

$$0.88 = t(2\pi r \times 0.3)r, t = \frac{0.467}{r^2}, \frac{dV}{dy} = \frac{t}{\mu} = \frac{0.467}{\mu r^2}, \int_{V_{\text{outer}}}^{V_{\text{inner}}} dV = \frac{0.467}{\mu} \int_{0.13}^{0.12} -\frac{dr}{r^2}, V_{\text{inner}} - V_{\text{outer}} = \frac{0.467}{\mu} \left[ \frac{1}{r} \right]_{0.13}^{0.12}$$

$$V_{\text{inner}} = 2\pi \times 0.12 = 0.754 \text{ m/s. } (0.754 - 0) = \frac{0.467}{\mu} \left[ \frac{1}{0.12} - \frac{1}{0.13} \right], \Rightarrow \mu = 0.397 \text{ Pas}$$

71. Displacement thickness =  $\int_0^{\delta} \left(1 - \frac{u}{U}\right) dy = \int_0^{\delta} \left[1 - \frac{2y}{\delta} + \left(\frac{y}{\delta}\right)^2\right] dy = \frac{\delta}{3}$

73. Mass of flywheel rim,  $m_r = \frac{2KE}{r^2(\omega_1^2 - \omega_2^2)} = \frac{2 \times 0.90 \times 207 \times 10^3}{(0.915)^2 \left[ \left(\frac{2\pi \times 200}{60}\right)^2 - \left(\frac{2\pi \times 180}{60}\right)^2 \right]} = 69.6 \text{ kg}$

Total mass of flywheel =  $1.15 \times 69.6 = 80 \text{ kg}$ .

74. Co-efficient of speed fluctuation is  $C_s = \frac{\omega_1 - \omega_2}{\omega} = 0.105$

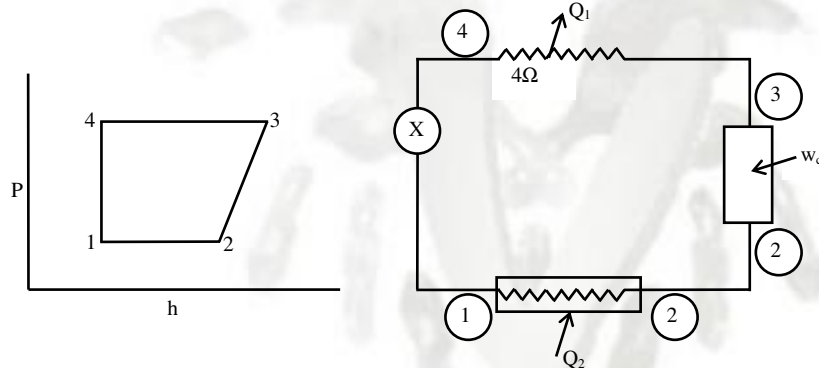
76-77.  $L_1 + L_2 + L_3 = 18 \Rightarrow k + 2k + 3k = 18, k = 3$

$L_1 = 3, L_2 = 6, L_3 = 9, d_1 \times d_2 \times d_3 = 20250 \Rightarrow 3k \times 2k \times k = 20250, k = 15$

$d_1 = 15 \text{ mm}, d_2 = 30 \text{ mm}, d_3 = 45 \text{ mm}, Q_1 = A_1 V_1 = \frac{\pi}{4} d_1^2 \times V_1 \Rightarrow V_1 = \frac{4Q_1}{\pi d_1^2}$ , Similarly  $V_2 = \frac{4Q_2}{\pi d_2^2}$  and  $V_3 = \frac{4Q_3}{\pi d_3^2}$

Head loss due to friction  $\frac{4fL_1 V_1^2}{d_1 \times 2g} = \frac{4fL_2 V_2^2}{d_2 \times 2g} + \frac{4fL_3 V_3^2}{d_3 \times 2g}$ , On solving above equation we get  $\frac{Q_3}{Q_2} = \frac{17}{3}$

78.



$h_1 = 80 \text{ kJ/kg}, h_2 = 200 \text{ kJ/kg}, h_3 = 220 \text{ kJ/kg},$

$\therefore h_4 = h_1 = 80 \text{ kJ/kg}, \text{mass flow rate} = \frac{5}{200 - 80} = 0.0417 \text{ kg/sec}$

79. Heat given by refrigerant in condenser =  $m(h_3 - h_4) = 0.0417 \times (220 - 80)$

80.  $D = \frac{mg\ell^3}{48I}, I = \frac{\pi}{64} \times (24)^4 = 16.3 \times 10^{-9} \text{ m}^4,$

$D = \frac{12 \times 9.81 \times (1)^3}{48 \times 2 \times 10^{11} \times 16.9 \times 10^{-9}} = 0.000752 \text{ m}, \omega_n = \sqrt{\frac{g}{D}} = 114.2 \text{ rad/sec.}$

81. Amplitude

$y = \frac{e}{\left(\frac{\omega_n}{\omega}\right)^2 - 1}, \omega = \frac{2\pi \times 2400}{60} = 251.32 \text{ rad/sec}, e = 0.11, y = 0.139 \text{ mm}$

82.  $9 \times 2.5 + 12 \times 6 \times 3 = 6 \times R_B$

$$R_B = 37.75 \text{ kN}$$

$$R_A + R_B = 12 \times 6 + 9$$

$$R_A = 41.25 \text{ kN}$$

$$\text{Shear force in section AC} = 41.25 - 12x$$

For maximum BM

$$41.25 - 12x = 0, x = 3.4375, x = 3.4375 \text{ does not lie in section AC}$$

Consider section BC

$$S_F = 41.25 - 12 \times -9$$

For Maximum B.M.  $S_F = 0$

$$x = 2.6875$$

$$\text{Now BM at } x = 2.6875 = 65.85 \text{ kNm}$$

83.  $M = z\sigma, z = \frac{M}{\sigma} = \frac{65.83 \times 10^6}{8} = 8.2287 \times 10^6, z = \frac{1}{6}bd^2 = \frac{1}{6}b(2b)^2 = \frac{2b^3}{3}$

$$\frac{2b^3}{3} = 8.2286 \times 10^6, b = 231 \text{ mm}, d = 462 \text{ mm} \therefore \text{cross sectional area} = 6 \times d = 0.231 \times 0.462 = 0.11 \text{ m}^2$$

84.  $\beta = \tan^{-1} \mu = \tan^{-1} (0.4) = 21.8^\circ, \alpha = 15^\circ$

$$\text{using equation } 2\phi + \beta - \alpha = \frac{\pi}{2} \Rightarrow 2\phi = 90^\circ - 21.8^\circ + 15^\circ = 83.2^\circ \Rightarrow \phi = 41.6^\circ$$

85.  $F_s = \frac{wt_1 \tau_s}{\sin \phi} = \frac{10 \times 0.1 \times 300}{\sin 41.6^\circ} = 451.86 \text{ N}, R = \frac{F_s}{\cos(\phi + \beta - \alpha)} = \frac{451.86}{\cos(41.6 + 21.8 - 15)} = 680.2 \text{ N}$

$$F_C = R \cos(\beta - \alpha) = 680.2 \times \cos(21.8 - 15) = 675.4 \text{ N}, F_t = R \sin(\beta - \alpha) = 680.2 \times \sin(21.8 - 15) = 80.54 \text{ N}$$